

## **TOOL08**

### Methodological tool

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Tool to determine the mass flow of a greenhouse gas in a gaseous stream

Version 03.0



**United Nations**  
Framework Convention on  
Climate Change

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## 1. Introduction

### 1.1. Background

1. This tool provides methodological guidance to determine the mass flow of greenhouse gases.

## 2. Scope, applicability, and entry into force

### 2.1. Scope

2. This tool provides procedures to determine the following parameter:

**Table 1. Parameters determined**

Parameter	SI Unit	Description
$F_{i,t}$	kg/h	Mass flow of greenhouse gas $i$ (CO <sub>2</sub> , CH <sub>4</sub> , N <sub>2</sub> O, SF <sub>6</sub> or a PFC) in the gaseous stream in time interval $t$

3. The mass flow of a particular greenhouse gas is calculated based on measurements of: (a) the total volume flow or mass flow of the gas stream, (b) the volumetric fraction of the gas in the gas stream and (c) the gas composition and water content. The flow and volumetric fraction may be measured on a **dry basis or wet basis**. The tool covers the possible measurement combinations, providing six different calculation options to determine the mass flow of a particular greenhouse gas (Options A to F shown in Table 2).
4. Additional guidance for determining the mass flow of methane in biogas is provided in the Appendix.

### 2.2. Applicability

5. Typical applications of this tool are methodologies where the flow and composition of residual or flared gases or exhaust gases are measured for the determination of baseline or project emissions.
6. Methodologies where CO<sub>2</sub> is the particular and only gas of interest should continue to adopt material balances as the means of flow determination and may not adopt this tool as material balances are the cost effective way of monitoring flow of CO<sub>2</sub>.
7. The underlying methodology should specify:
  - (a) The gaseous stream the tool should be applied to;
  - (b) For which greenhouse gases the mass flow should be determined;
  - (c) In which time intervals the flow of the gaseous stream should be measured; and
  - (d) Situations where the simplification offered for calculating the molecular mass of the gaseous stream (equations (3) or (17)) is not valid (such as the gaseous stream is predominantly composed of a gas other than N<sub>2</sub>).

### 2.3. Entry into force

8. The date of entry into force is the date of the publication of the EB 87 meeting report on 27 November 2015.

## 3. Normative references

9. Fundamentals of Classical Thermodynamics; Gordon J. Van Wylen, Richard E. Sonntag and Borgnakke; 4<sup>o</sup> Edition 1994, John Wiley & Sons, Inc.
10. Drying: Principles, Applications and Design; Czeslaw Strumillo and Tadeusz Kudra; 1986; Gordon & Breach Science Publisher; Montreaux, Switzerland.

## 4. Definitions

11. The definitions contained in the Glossary of CDM terms shall apply.
12. For the purpose of this tool, the following definitions apply:
  - (a) **Absolute humidity** - the ratio between the mass of H<sub>2</sub>O (vapor phase) in the gas and the mass of the dry gas;
  - (b) **Dry basis** - a parameter that does not account for the H<sub>2</sub>O present in the gas;
  - (c) **Gaseous stream** - a mixture of gaseous components which may contain different fractions of N<sub>2</sub>, CO<sub>2</sub>, O<sub>2</sub>, CO, H<sub>2</sub>, CH<sub>4</sub>, N<sub>2</sub>O, NO, NO<sub>2</sub>, SO<sub>2</sub>, SF<sub>6</sub>, PFCs and H<sub>2</sub>O in the vapor phase and its absolute pressure must be below 10 atm or 1.013 MPa.<sup>1</sup> Other gases may be present (e.g. hydrocarbons) provided their total concentration represents less than 1% (v/v) of the total.<sup>2</sup> A dry gas or dry gaseous stream excludes the H<sub>2</sub>O fraction and a wet gas or wet gaseous stream includes the H<sub>2</sub>O fraction;
  - (d) **Moisture content** - the H<sub>2</sub>O concentration in mass of H<sub>2</sub>O (vapor phase) per volume of dry gas at normal conditions, also referred to as NPT conditions, expressed in mg H<sub>2</sub>O/m<sup>3</sup> dry gas;
  - (e) **Normal conditions** - as 0°C (273.15 K, 32°F) and 1 atm (101.325 kN/m<sup>2</sup>, 101.325 kPa, 14.69 psia, 29.92 in Hg, 760 torr);
  - (f) **Relative humidity** - the ratio between the partial pressure of H<sub>2</sub>O in the gas and the saturation pressure at a given temperature;
  - (g) **Saturation (absolute) humidity** - the maximum amount of H<sub>2</sub>O (vapor phase) that the gas can contain at a given temperature and pressure, expressed as mass of H<sub>2</sub>O per mass of the dry gas;

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<sup>1</sup> This condition is required because it is assumed in the calculations that the gas stream behaves as an ideal binary mixture of water vapor and an ideal gas. If the gaseous stream contains larger fractions of other gases, such as hydrocarbons other than methane or HFCs, the gas cannot be considered to be an ideal gas mixture. Moderate pressures will assure that gases behave as ideal gases.

<sup>2</sup> For the cases of landfill gas and exhaust gases from thermal oxidation using natural gas, it will be assumed that the total concentration of other gases represents less than 1% (v/v).

- (h) **Wet basis** - a parameter that accounts for the H<sub>2</sub>O present in the gas.

## 5. Methodology procedure

13. The mass flow of a greenhouse gas  $i$  in a gaseous stream ( $F_{i,t}$ ) is determined through measurement of the flow and volumetric fraction of the gaseous stream. Table 2 shows the different ways to make these measurements and the corresponding calculation option for  $F_{i,t}$ .
14. Project participants should document in the CDM-PDD which option is applied.  $F_{i,t}$  should be calculated following the steps/guidance described for each option below.

**Table 2. Measurement options**

Option	Flow of gaseous stream	Volumetric fraction
A	Volume flow – dry basis	dry or wet basis <sup>3</sup>
B	Volume flow – wet basis	dry basis
C	Volume flow – wet basis	wet basis
D	Mass flow – dry basis	dry or wet basis
E	Mass flow – wet basis	dry basis
F	Mass flow – wet basis	wet basis

### 5.1. Determination of the absolute humidity of the gaseous stream

15. The absolute humidity is a parameter required for Options B and E. It can be determined from measurement of the moisture content (Option 1), or by assuming the gaseous stream is dry or saturated in a simplified conservative approach (Option 2). Project participants should document in the CDM-PDD which option they apply.

#### 5.1.1. Option 1: Calculation using measurement of the moisture content

16. This option provides a procedure to determine the absolute humidity of the gaseous stream ( $m_{H_2O,t,db}$ ) from measurements of the moisture content of the gas, according to equation (1).

$$m_{H_2O,t,db} = \frac{C_{H_2O,t,db,n}}{10^6 \times \rho_{t,db,n}} \quad \text{Equation (1)}$$

Where:

$m_{H_2O,t,db}$  = Absolute humidity of the gaseous stream in time interval  $t$  on a dry basis (kg H<sub>2</sub>O/kg dry gas)

$C_{H_2O,t,db,n}$  = Moisture content of the gaseous stream in time interval  $t$  on a dry basis at normal conditions (mg H<sub>2</sub>O/m<sup>3</sup> dry gas)

<sup>3</sup> Flow measurement on a dry basis is not feasible at reasonable costs for a wet gaseous stream, so there will be no difference in the readings for volumetric fraction in wet basis analyzers and dry basis analyzers and both types can be used indistinctly for calculation Options A and D.

$\rho_{t,db,n}$  = Density of the gaseous stream in time interval  $t$  on a dry basis at normal conditions (kg dry gas/m<sup>3</sup> dry gas)

17. The density of the gaseous stream on a dry basis at normal conditions ( $\rho_{t,db,n}$ ) is determined as follows:

$$\rho_{t,db,n} = \frac{P_n \times MM_{t,db}}{R_u \times T_n} \quad \text{Equation (2)}$$

Where:

$\rho_{t,db,n}$  = Density of the gaseous stream in time interval  $t$  on a dry basis at normal conditions (kg dry gas/m<sup>3</sup> dry gas)

$P_n$  = Absolute pressure at normal conditions (Pa)

$T_n$  = Temperature at normal conditions (K)

$MM_{t,db}$  = Molecular mass of the gaseous stream in a time interval  $t$  on a dry basis (kg dry gas/kmol dry gas)

$R_u$  = Universal ideal gases constant (Pa.m<sup>3</sup>/kmol.K)

18. The molecular mass of the gaseous stream ( $MM_{t,db}$ ) is estimated as follows:

$$MM_{t,db} = \sum_k (v_{k,t,db} \times MM_k) \quad \text{Equation (3)}$$

Where:

$MM_{t,db}$  = Molecular mass of the gaseous stream in time interval  $t$  on a dry basis (kg dry gas/kmol dry gas)

$v_{k,t,db}$  = Volumetric fraction of gas  $k$  in the gaseous stream in time interval  $t$  on a dry basis (m<sup>3</sup> gas k/m<sup>3</sup> dry gas)

$MM_k$  = Molecular mass of gas  $k$  (kg/kmol)

$k$  = All gases, except H<sub>2</sub>O, contained in the gaseous stream (e.g. N<sub>2</sub>, CO<sub>2</sub>, O<sub>2</sub>, CO, H<sub>2</sub>, CH<sub>4</sub>, N<sub>2</sub>O, NO, NO<sub>2</sub>, SO<sub>2</sub>, SF<sub>6</sub> and PFCs). See available simplification below

19. The determination of the molecular mass of the gaseous stream ( $MM_{t,db}$ ) requires measuring the volumetric fraction of all gases ( $k$ ) in the gaseous stream. However as a simplification, the volumetric fraction of only the gases  $k$  that are greenhouse gases and are considered in the emission reduction calculation in the underlying methodology must be monitored and the difference to 100% may be considered as pure nitrogen. The simplification is not acceptable if it is differently specified in the underlying methodology.

### 5.1.2. Option 2: Simplified calculation without measurement of the moisture content

20. This option provides a simple and conservative approach to determine the absolute humidity by assuming the gaseous stream is dry or saturated depending on which is the conservative situation.<sup>4</sup>
21. If it is conservative to assume that the gaseous stream is dry, then  $m_{H_2O,t,db}$  is assumed to equal 0. If it is conservative to assume that the gaseous stream is saturated, then  $m_{H_2O,t,db}$  is assumed to equal the saturation absolute humidity ( $m_{H_2O,t,db,sat}$ ) and calculated using equation (4).

$$m_{H_2O,t,db,sat} = \frac{p_{H_2O,t,Sat} \times MM_{H_2O}}{(P_t - p_{H_2O,t,Sat}) \times MM_{t,db}} \quad \text{Equation (4)}$$

Where:

$m_{H_2O,t,db,sat}$	=	Saturation absolute humidity in time interval $t$ on a dry basis (kg H <sub>2</sub> O/kg dry gas)
$p_{H_2O,t,Sat}$	=	Saturation pressure of H <sub>2</sub> O at temperature $T_t$ in time interval $t$ (Pa)
$T_t$	=	Temperature of the gaseous stream in time interval $t$ (K)
$P_t$	=	Absolute pressure of the gaseous stream in time interval $t$ (Pa)
$MM_{H_2O}$	=	Molecular mass of H <sub>2</sub> O (kg H <sub>2</sub> O/kmol H <sub>2</sub> O)
$MM_{t,db}$	=	Molecular mass of the gaseous stream in a time interval $t$ on a dry basis (kg dry gas/kmol dry gas)

22. Parameter  $MM_{t,db}$  is estimated using equation (3).

#### 5.1.2.1. Option A

23. Flow measurement on a dry basis is not doable for a wet gaseous stream. Therefore, it is necessary to demonstrate that the gaseous stream is dry to use this option. There are two ways to do this:
- Measure the moisture content of the gaseous stream ( $C_{H_2O,t,db,n}$ ) and demonstrate that this is less or equal to 0.05 kg H<sub>2</sub>O/m<sup>3</sup> dry gas; or
  - Demonstrate that the temperature of the gaseous stream ( $T_t$ ) is less than 60°C (333.15 K) at the flow measurement point.
24. If it cannot be demonstrated that the gaseous stream is dry, then the flow measurement should be assumed to be on a wet basis and the corresponding option from Table 2 should be applied instead.

<sup>4</sup> An assumption that the gaseous stream is saturated is conservative for the situation that the mass flow of greenhouse gas  $i$  is underestimated (applicable for calculating baseline emissions). Conversely, an assumption that the gas stream is dry is conservative for the situation that the greenhouse gas  $i$  is overestimated (applicable for calculating project emissions).

25. The mass flow of greenhouse gas  $i$  ( $F_{i,t}$ ) is determined as follows:

$$F_{i,t} = V_{t,db} \times v_{i,t,db} \times \rho_{i,t} \quad \text{Equation (5)}$$

With:

$$\rho_{i,t} = \frac{P_t \times MM_i}{R_u \times T_t} \quad \text{Equation (6)}$$

Where:

$F_{i,t}$	=	Mass flow of greenhouse gas $i$ in the gaseous stream in time interval $t$ (kg gas/h)
$V_{t,db}$	=	Volumetric flow of the gaseous stream in time interval $t$ on a dry basis (m <sup>3</sup> dry gas/h)
$v_{i,t,db}$	=	Volumetric fraction of greenhouse gas $i$ in the gaseous stream in a time interval $t$ on a dry basis (m <sup>3</sup> gas $i$ /m <sup>3</sup> dry gas)
$\rho_{i,t}$	=	Density of greenhouse gas $i$ in the gaseous stream in time interval $t$ (kg gas $i$ /m <sup>3</sup> gas $i$ )
$P_t$	=	Absolute pressure of the gaseous stream in time interval $t$ (Pa)
$MM_i$	=	Molecular mass of greenhouse gas $i$ (kg/kmol)
$R_u$	=	Universal ideal gases constant (Pa.m <sup>3</sup> /kmol.K)
$T_t$	=	Temperature of the gaseous stream in time interval $t$ (K)

### 5.1.2.2. Option B

26. The mass flow of greenhouse gas  $i$  ( $F_{i,t}$ ) is determined using equations (5) and (6). The volumetric flow of the gaseous stream in time interval  $t$  on a dry basis ( $V_{t,db}$ ) is determined by converting the measured volumetric flow from wet basis to dry basis as follows:

$$V_{t,db} = V_{t,wb} / (1 + v_{H_2O,t,db}) \quad \text{Equation (7)}$$

Where:

$V_{t,db}$	=	Volumetric flow of the gaseous stream in time interval $t$ on a dry basis (m <sup>3</sup> dry gas/h)
$V_{t,wb}$	=	Volumetric flow of the gaseous stream in time interval $t$ on a wet basis (m <sup>3</sup> wet gas/h)
$v_{H_2O,t,db}$	=	Volumetric fraction of H <sub>2</sub> O in the gaseous stream in time interval $t$ on a dry basis (m <sup>3</sup> H <sub>2</sub> O/m <sup>3</sup> dry gas)

27. The volumetric fraction of H<sub>2</sub>O in time interval  $t$  on a dry basis ( $v_{H_2O,t,db}$ ) is estimated according to equation (8).



$$v_{H_2O,t,db} = \frac{m_{H_2O,t,db} \times MM_{t,db}}{MM_{H_2O}} \quad \text{Equation (8)}$$

Where:

$v_{H_2O,t,db}$	=	Volumetric fraction of H <sub>2</sub> O in the gaseous stream in time interval $t$ on a dry basis (m <sup>3</sup> H <sub>2</sub> O/m <sup>3</sup> dry gas)
$m_{H_2O,t,db}$	=	Absolute humidity in the gaseous stream in time interval $t$ on a dry basis (kg H <sub>2</sub> O/kg dry gas)
$MM_{t,db}$	=	Molecular mass of the gaseous stream in time interval $t$ on a dry basis (kg dry gas/kmol dry gas)
$MM_{H_2O}$	=	Molecular mass of H <sub>2</sub> O (kg H <sub>2</sub> O/kmol H <sub>2</sub> O)

28. The absolute humidity of the gaseous stream ( $m_{H_2O,t,db}$ ) is determined using either Option 1 or 2 specified in the Determination of the absolute humidity of the gaseous stream section of the tool and the molecular mass of the gaseous stream ( $MM_{t,db}$ ) is determined using equation (3).

### 5.1.2.3. Option C

29. The mass flow of greenhouse gas  $i$  ( $F_{i,t}$ ) is determined as follows:

$$F_{i,t} = V_{t,wb,n} \times v_{i,t,wb} \times \rho_{i,n} \quad \text{Equation (9)}$$

With:

$$\rho_{i,n} = \frac{P_n \times MM_i}{R_u \times T_n} \quad \text{Equation (10)}$$

Where:

$F_{i,t}$	=	Mass flow of greenhouse gas $i$ in the gaseous stream in time interval $t$ (kg gas/h)
$V_{t,wb,n}$	=	Volumetric flow of the gaseous stream in time interval $t$ on a wet basis at normal conditions (m <sup>3</sup> wet gas/h)
$v_{i,t,wb}$	=	Volumetric fraction of greenhouse gas $i$ in the gaseous stream in time interval $t$ on a wet basis (m <sup>3</sup> gas $i$ /m <sup>3</sup> wet gas)
$\rho_{i,n}$	=	Density of greenhouse gas $i$ in the gaseous stream at normal conditions (kg gas $i$ /m <sup>3</sup> wet gas $i$ )
$P_n$	=	Absolute pressure at normal conditions (Pa)
$T_n$	=	Temperature at normal conditions (K)
$MM_i$	=	Molecular mass of greenhouse gas $i$ (kg/kmol)
$R_u$	=	Universal ideal gases constant (Pa.m <sup>3</sup> /kmol.K)

30. The following equation should be used to convert the volumetric flow of the gaseous stream from actual conditions to normal conditions of temperature and pressure:

$$V_{t,wb,n} = V_{t,wb} \times [(T_n/T_t) \times (P_t/P_n)] \quad \text{Equation (11)}$$

Where:

$V_{t,wb,n}$	=	Volumetric flow of the gaseous stream in a time interval $t$ on a wet basis at normal conditions ( $\text{m}^3$ wet gas/h)
$V_{t,wb}$	=	Volumetric flow of the gaseous stream in time interval $t$ on a wet basis ( $\text{m}^3$ wet gas/h)
$P_t$	=	Pressure of the gaseous stream in time interval $t$ (Pa)
$T_t$	=	Temperature of the gaseous stream in time interval $t$ (K)
$P_n$	=	Absolute pressure at normal conditions (Pa)
$T_n$	=	Temperature at normal conditions (K)

#### 5.1.2.4. Option D

31. Flow measurement on a dry basis is not doable for a wet gaseous stream. Therefore, it is necessary to demonstrate that the gaseous stream is dry to use this option. There are two ways to do this:
- Measure the moisture content of the gaseous stream ( $C_{\text{H}_2\text{O},t,db,n}$ ) and demonstrate that this is less or equal to  $0.05 \text{ kg H}_2\text{O}/\text{m}^3$  dry gas; or
  - Demonstrate that the temperature of the gaseous stream ( $T_t$ ) is less than  $60^\circ\text{C}$  ( $333.15 \text{ K}$ ) at the flow measurement point.
32. If it cannot be demonstrated that the gaseous stream is dry, then the flow measurement should be assumed to be on a wet basis and the corresponding option from Table 2 should be applied instead.
33. The mass flow of greenhouse gas  $i$  ( $F_{i,t}$ ) is determined using equations (5) and (6). The volumetric flow of the gaseous stream in time interval  $t$  on a dry basis ( $V_{t,db}$ ) is determined by converting the mass flow of the gaseous stream to a volumetric flow as follows:

$$V_{t,db} = M_{t,db} / \rho_{t,db} \quad \text{Equation (12)}$$

Where:

$V_{t,db}$	=	Volumetric flow of the gaseous stream in time interval $t$ on a dry basis ( $\text{m}^3$ dry gas/h)
$M_{t,db}$	=	Mass flow of the gaseous stream in time interval $t$ on a dry basis (kg/h)
$\rho_{t,db}$	=	Density of the gaseous stream in time interval $t$ on a dry basis ( $\text{kg dry gas}/\text{m}^3$ dry gas)

34. The density of the gaseous stream ( $\rho_{t,db}$ ) should be determined as follows:

$$\rho_{t,db} = \frac{P_t \times MM_{t,db}}{R_u \times T_t} \quad \text{Equation (13)}$$

Where:

- $\rho_{t,db}$  = Density of the gaseous stream in a time interval  $t$  on a dry basis (kg dry gas/m<sup>3</sup> dry gas)
- $MM_{t,db}$  = Molecular mass of the gaseous stream in a time interval  $t$  on a dry basis (kg dry gas/kmol dry gas)
- $P_t$  = Pressure of the gaseous stream in time interval  $t$  (Pa)
- $T_t$  = Temperature of the gaseous stream in time interval  $t$  (K)

35. The molecular mass of the gaseous stream ( $MM_{t,db}$ ) is estimated using equation (3).

#### 5.1.2.5. Option E

36. The mass flow of greenhouse gas  $i$  ( $F_{i,t}$ ) is determined using equations (5) and (6). The volumetric flow of the gaseous stream in time interval  $t$  on a dry basis ( $V_{t,db}$ ) is determined in two steps. First the mass flow of the gaseous stream in time interval  $t$  on a wet basis ( $M_{t,wb}$ ) is converted from wet basis to dry basis as follows:

$$M_{t,db} = M_{t,wb} / (1 + m_{H_2O,t,db}) \quad \text{Equation (14)}$$

Where:

- $M_{t,db}$  = Mass flow of the gaseous stream in time interval  $t$  on a dry basis (kg/h)
- $M_{t,wb}$  = Mass flow of the gaseous stream in time interval  $t$  on a wet basis (kg/h)
- $m_{H_2O,t,db}$  = Absolute humidity of H<sub>2</sub>O in the gaseous stream in a time interval  $t$  on a dry basis (kg H<sub>2</sub>O/kg dry gas)

37. Then, the mass flow of the gaseous stream in time interval  $t$  on a dry basis ( $M_{t,db}$ ) is converted to the volumetric flow of the gaseous stream in time interval  $t$  on a dry basis ( $V_{t,db}$ ) using equation (12).

38. The absolute humidity of the gaseous stream ( $m_{H_2O,t,db}$ ) is determined using either Option 1 or 2 specified in the "Determination of the absolute humidity of the gaseous stream" section of the tool.

#### 5.1.2.6. Option F

39. The mass flow of greenhouse gas  $i$  ( $F_{i,t}$ ) is determined using equations (9), (10), and the following equations:

$$V_{t,wb,n} = M_{t,wb} / \rho_{t,wb,n} \quad \text{Equation (15)}$$

And

$$\rho_{t,wb,n} = \frac{P_n \times MM_{t,wb}}{R_u \times T_n} \quad \text{Equation (16)}$$

Where:

$V_{t,wb,n}$	=	Volumetric flow of the gaseous stream in time interval $t$ at normal conditions on a wet basis ( $\text{m}^3$ wet gas/h)
$V_{i,t,wb}$	=	Volumetric fraction of greenhouse gas $i$ in the gaseous stream in time interval $t$ on a wet basis ( $\text{m}^3$ gas $i/\text{m}^3$ wet gas)
$M_{t,wb}$	=	Mass flow of the gaseous stream in time interval $t$ on a wet basis (kg/h)
$\rho_{t,wb,n}$	=	Density of the gaseous stream in time interval $t$ on a wet basis at normal conditions (kg wet gas/ $\text{m}^3$ wet gas)
$P_n$	=	Absolute pressure at normal conditions (Pa)
$T_n$	=	Temperature at normal conditions (K)
$MM_{t,wb}$	=	Molecular mass of the gaseous stream in time interval $t$ on a wet basis (kg wet gas/kmol wet gas)
$R_u$	=	Universal ideal gases constant ( $\text{Pa}\cdot\text{m}^3/\text{kmol}\cdot\text{K}$ )

40. The molecular mass of the gaseous stream ( $MM_{t,wb}$ ) is determined as follows:

$$MM_{t,wb} = \sum_k (V_{k,t,wb} \times MM_k) \quad \text{Equation (17)}$$

Where:

$MM_{t,wb}$	=	Molecular mass of the gaseous stream in time interval $t$ on a wet basis (kg wet gas/kmol wet gas)
$V_{k,t,wb}$	=	Volumetric fraction of gas $k$ in the gaseous stream in time interval $t$ on a wet basis ( $\text{m}^3$ gas $k/\text{m}^3$ wet gas)
$MM_k$	=	Molecular mass of gas $k$ (kg/kmol)
$k$	=	All gases contained in the gaseous stream (e.g. $\text{N}_2$ , $\text{CO}_2$ , $\text{O}_2$ , $\text{CO}$ , $\text{H}_2$ , $\text{CH}_4$ , $\text{N}_2\text{O}$ , $\text{NO}$ , $\text{NO}_2$ , $\text{SO}_2$ , $\text{SF}_6$ and PFCs and $\text{H}_2\text{O}$ in vapor phase). See available simplification below

41. The determination of the molecular mass of the gaseous stream ( $MM_{t,wb}$ ) requires measuring the volumetric fraction of all gases ( $k$ ) in the gaseous stream. However as a simplification, the volumetric fraction of only the gases  $k$  that are greenhouse gases and are considered in the emission reduction calculation in the underlying methodology must be monitored and the difference to 100% may be considered as pure nitrogen. The simplification is not acceptable if it is differently specified in the underlying methodology.

## 5.2. Data and parameters not monitored

Data / Parameter table 1.

Data / Parameter:	$R_u$
Data unit:	Pa.m <sup>3</sup> /kmol.K
Description:	Universal ideal gases constant
Value to be applied:	8,314
Any comment:	

Data / Parameter table 2.

Data / Parameter:	$MM_i$																																						
Data unit:	kg/kmol																																						
Description:	Molecular mass of greenhouse gas <i>i</i>																																						
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Any comment:																																							

Data / Parameter table 3.

Data / Parameter:	$MM_k$
Data unit:	kg/kmol
Description:	Molecular mass of gas <i>k</i>

Value to be applied:	For gases $k$ that are greenhouse gases apply values for $MM_i$ .		
	<b>Compound</b>	<b>Structure</b>	<b>Molecular mass (kg / kmol)</b>
	Nitrogen	N <sub>2</sub>	28.01
	Oxygen	O <sub>2</sub>	32.00
	Carbon monoxide	CO	28.01
	Hydrogen	H <sub>2</sub>	2.02
	Nitric oxide	NO	30.01
	Nitrogen dioxide	NO <sub>2</sub>	46.01
	Sulfur dioxide	SO <sub>2</sub>	64.06
Any comment:			

**Data / Parameter table 4.**

<b>Data / Parameter:</b>	$MM_{H_2O}$
Data unit:	kg/kmol
Description:	Molecular mass of water
Value to be applied:	18.0152 kg/kmol
Any comment:	

**Data / Parameter table 5.**

<b>Data / Parameter:</b>	$P_n$
Data unit:	Pa
Description:	Total pressure at normal conditions
Value to be applied:	101,325 Pa
Any comment:	

**Data / Parameter table 6.**

<b>Data / Parameter:</b>	$T_n$
Data unit:	K
Description:	Temperature at normal conditions
Value to be applied:	273.15 K
Any comment:	

## 6. Monitoring methodology

### 6.1. Data and parameters to be monitored

42. All monitored data must be linked in time, i.e. calculations shall be performed considering only a set of data acquired in the same time interval. As noted above, project participants may use an hour or a smaller discrete time interval. Furthermore, additional guidance is provided in the Appendix for the purpose of monitoring mass flow of methane in the biogas.

**Data / Parameter table 7.**

<b>Data / Parameter:</b>	$V_{t,wb}$
Data unit:	m <sup>3</sup> wet gas/h
Description:	Volumetric flow of the gaseous stream in time interval $t$ on a wet basis
Source of data:	
Measurement procedures (if any):	Volumetric flow measurement should always refer to the actual pressure and temperature. Instruments with recordable electronic signal (analogical or digital) are required
Monitoring frequency:	Continuous if not specified in the underlying methodology
QA/QC procedures:	Periodic calibration against a primary device provided by an independent accredited laboratory is mandatory for all projects applying large scale methodology(ies). Calibration and frequency of calibration is according to manufacturer's specifications
Any comment:	This parameter will be monitored in Options B and C

**Data / Parameter table 8.**

<b>Data / Parameter:</b>	$V_{t,db}$
Data unit:	m <sup>3</sup> dry gas/h
Description:	Volumetric flow of the gaseous stream in time interval $t$ on a dry basis
Source of data:	
Measurement procedures (if any):	Volumetric flow measurement should always refer to the actual pressure and temperature. Calculated based on the wet basis flow measurement plus water concentration measurement
Monitoring frequency:	Continuous if not specified in the underlying methodology
QA/QC procedures:	Periodic calibration against a primary device provided by an independent accredited laboratory is mandatory for all projects applying large scale methodology(ies). Calibration and frequency of calibration is according to manufacturer's specifications
Any comment:	This parameter will be monitored in Options A

**Data / Parameter table 9.**

<b>Data / Parameter:</b>	$V_{i,t,db}$
Data unit:	m <sup>3</sup> gas $i$ /m <sup>3</sup> dry gas
Description:	Volumetric fraction of greenhouse gas $i$ in a time interval $t$ on a dry basis
Source of data:	
Measurement procedures (if any):	Continuous gas analyser operating in dry-basis. Volumetric flow measurement should always refer to the actual pressure and temperature
Monitoring frequency:	Continuous if not specified in the underlying methodology

QA/QC procedures:	Calibration should include zero verification with an inert gas (e.g. N <sub>2</sub> ) and at least one reading verification with a standard gas (single calibration gas or mixture calibration gas). All calibration gases must have a certificate provided by the manufacturer and must be under their validity period.
Any comment:	This parameter will be monitored in Options B and E and may be monitored in Options A and D

**Data / Parameter table 10.**

<b>Data / Parameter:</b>	$V_{i,t,wb}$
Data unit:	m <sup>3</sup> gas <i>i</i> /m <sup>3</sup> wet gas
Description:	Volumetric fraction of greenhouse gas <i>i</i> in a time interval <i>t</i> on a wet basis
Source of data:	
Measurement procedures (if any):	Calculated based on the dry basis analysis plus water concentration measurement or continuous in-situ analyzers if not specified in the underlying methodology
Monitoring frequency:	Continuous if not specified in the underlying methodology
QA/QC procedures:	Calibration should include zero verification with an inert gas (e.g. N <sub>2</sub> ) and at least one reading verification with a standard gas (single calibration gas or mixture calibration gas). All calibration gases must have a certificate provided by the manufacturer and must be under their validity period.
Any comment:	This parameter will be monitored in Options C and F and may be monitored in Options A and D

**Data / Parameter table 11.**

<b>Data / Parameter:</b>	$M_{t,wb}$
Data unit:	kg/h
Description:	Mass flow of the gaseous stream in time interval <i>t</i> on a wet basis
Source of data:	
Measurement procedures (if any):	Instruments with recordable electronic signal (analogical or digital) are required
Monitoring frequency:	Continuous if not specified in the underlying methodology
QA/QC procedures:	Periodic calibration against a primary device provided by an independent accredited laboratory is mandatory. Calibration and frequency of calibration is according to manufacturer's specifications
Any comment:	This parameter will be monitored in Options E and F

**Data / Parameter table 12.**

<b>Data / Parameter:</b>	$M_{t,db}$
Data unit:	kg/h
Description:	Mass flow of the gaseous stream in time interval <i>t</i> on a dry basis
Source of data:	



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Measurement procedures (if any):	Calculated based on the wet basis flow measurement plus water concentration measurement
Monitoring frequency:	Continuous if not specified in the underlying methodology
QA/QC procedures:	Calibration and frequency of calibration is according to manufacturer's specifications
Any comment:	This parameter will be monitored in Option D

**Data / Parameter table 13.**

<b>Data / Parameter:</b>	$C_{H_2O,t,db,n}$
Data unit:	mg H <sub>2</sub> O/m <sup>3</sup> dry gas
Description:	Moisture content of the gaseous stream at normal conditions, in time interval <i>t</i>
Source of data:	Measurements according to the USEPA CF42 method 4 – Gravimetric determination of water content
Measurement procedures (if any):	Discrete measurement procedure
Monitoring frequency:	The mean value among three consecutive measurements performed in the same day (at least 2 hours each) shall be considered. Measurements should coincide with the Annual Surveillance Test (associated with requirements of the EN 14181 standard) or the calibration of the flow meter for the gaseous stream
QA/QC procedures:	According to the USEPA CF42 method 4
Any comment:	Monitoring is required if Option 1 described in the “Determination of the absolute humidity of the gaseous stream” section of the tool is applied, or as one of the ways of proving that the gaseous stream is dry (necessary for Options A or D)

**Data / Parameter table 14.**

<b>Data / Parameter:</b>	$T_t$
Data unit:	K
Description:	Temperature of the gaseous stream in time interval <i>t</i>
Source of data:	
Measurement procedures (if any):	Instruments with recordable electronic signal (analogical or digital) are required. Examples include thermocouples, thermo resistance, etc
Monitoring frequency:	Continuous unless differently specified in the underlying methodology
QA/QC procedures:	Periodic calibration against a primary device provided by an independent accredited laboratory is mandatory. Calibration and frequency of calibration is according to manufacturer's specifications
Any comment:	Provided all parameters are converted to normal conditions during the monitoring process, this parameter may not be needed except for moisture content determination and therefore it should be metered only when performing such measurements (with same frequency). However, if the applicability condition related to the gaseous stream flow temperature being below 60°C is adopted, this parameter must be monitored continuously to assure the applicability condition is met

**Data / Parameter table 15.**

<b>Data / Parameter:</b>	$P_t$
Data unit:	Pa
Description:	Pressure of the gaseous stream in time interval $t$
Source of data:	
Measurement procedures (if any):	Instruments with recordable electronic signal (analogical or digital) are required. Examples include pressure transducers, etc
Monitoring frequency:	Continuous unless differently specified in the underlying methodology
QA/QC procedures:	Periodic calibration against a primary device must be performed periodically and records of calibration procedures must be kept available as well as the primary device and its calibration certificate. Pressure transducers (either capacitive or resistive) must be calibrated monthly
Any comment:	Provided all parameters are converted to normal conditions during the monitoring process, this parameter may not be needed except for moisture content determination and therefore it should be metered only when performing such measurements (with same frequency)

**Data / Parameter table 16.**

<b>Data / Parameter:</b>	$p_{H_2O,t,Sat}$
Data unit:	Pa
Description:	Saturation pressure of H <sub>2</sub> O at temperature $T_t$ in time interval $t$
Source of data:	
Measurement procedures (if any):	This parameter is solely a function of the gaseous stream temperature $T_t$ and can be found at reference [1] for a total pressure equal to 101,325 Pa
Monitoring frequency:	
QA/QC procedures:	
Any comment:	[1] Fundamentals of Classical Thermodynamics; Gordon J. Van Wylen, Richard E. Sonntag and Borgnakke; 4 <sup>o</sup> Edition 1994, John Wiley & Sons, Inc.

**Data / Parameter table 17.**

<b>Data / Parameter:</b>	$V_{k,t,db}$
Data unit:	m <sup>3</sup> gas k/m <sup>3</sup> dry gas
Description:	Volumetric fraction of gas $k$ in the gaseous stream in time interval $t$ on a dry basis
Source of data:	
Measurement procedures (if any):	Continuous gas analyser operating in dry-basis
Monitoring frequency:	Continuous if not specified in the underlying methodology/tool

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QA/QC procedures:	Calibration should include zero verification with an inert gas (e.g. N <sub>2</sub> ) and at least one reading verification with a standard gas (single calibration gas or mixture calibration gas). All calibration gases must have a certificate provided by the manufacturer and must be under their validity period
Any comment:	

**Data / Parameter table 18.**

<b>Data / Parameter:</b>	<b><math>V_{k,t,wb}</math></b>
Data unit:	m <sup>3</sup> gas k/m <sup>3</sup> wet gas
Description:	Volumetric fraction of gas <i>k</i> in the gaseous stream in time interval <i>t</i> on a wet basis
Source of data:	
Measurement procedures (if any):	Calculated based on the dry basis analysis plus water concentration measurement or continuous in-situ analyzers if not specified in the underlying methodology/tool
Monitoring frequency:	Continuous if not specified in the underlying methodology
QA/QC procedures:	Calibration should include zero verification with an inert gas (e.g. N <sub>2</sub> ) and at least one reading verification with a standard gas (single calibration gas or mixture calibration gas). All calibration gases must have a certificate provided by the manufacturer and must be under their validity period
Any comment:	

**Data / Parameter table 19.**

<b>Data / Parameter:</b>	<b>Status of biogas destruction device</b>
Data unit:	
Description:	Operational status of biogas destruction devices
Source of data:	
Measurement procedures (if any):	Monitoring and documenting may be undertaken by recording the energy production from methane captured or the operation of the flare by means of a flame detector to demonstrate the actual destruction of methane, unless a different method is specified in the underlying methodology/tool. Emission reductions will not accrue for periods in which the destruction device is not operational.
Monitoring frequency:	Continuous if not specified in the underlying methodology/tool
QA/QC procedures:	
Any comment:	For Flame detector devices refer to the methodological tool "Project emissions from flaring"

## Appendix. Additional data handling and monitoring guidance for determining the mass flow of methane in biogas

1. This appendix is applicable small-scale and large-scale project activities to the determination of mass flow of methane in biogas from waste treatment and landfill gas.

### 1. Data substitution for methane content or biogas flow

2. If missing data are encountered in the course of determining the methane mass flow, it may be substituted with conservative data sets (see below) from specific periods. However, data substitution shall only be applied to either the methane concentration or the biogas volumetric flow readings, but not to both simultaneously. If data is missing for both parameters during a given period of time, no data substitution shall be allowed for that period.

3. Substitution as outlined in Table 1 below may be undertaken only if the following conditions are met:

- (a) For methane concentration, biogas flow rates during the period where data gap occurred (data gap period) shall be consistent with normal operation (i.e. the average flow rates during the gap period shall not deviate from the average flow rates of the period taken for data substitution (data substitution period)<sup>1</sup> by more than +/- 20%); and
- (b) For biogas flow rate, methane concentration during the data gap period shall be consistent with the methane concentration observed during normal operations (i.e. the average methane concentration during the data gap period shall not deviate from the average methane concentration of the data substitution period by more than +/- 20%); and
- (c) Project participants shall demonstrate that the methane is being destroyed during the period of the data gap. If corroborating parameters fail to demonstrate any of these requirements, no substitution shall be allowed.

**Table 1. Data substitution procedure**

Duration of Missing Data	Data Substitution procedure
Less than six hours	Use the weighted average of the four hours period immediately before and four hours period immediately after the outage
Six to 24 hours	Use the upper bound or lower bound of 95% confidence interval of the data spanning 24 hours prior to and 24 hours after the outage, whichever results in more conservative estimate of emission reductions

<sup>1</sup> The data substitution period is determined as detailed in data substitution procedure in table 1 below

Duration of Missing Data	Data Substitution procedure
One to seven days	Use the upper bound or lower bound of 95% confidence interval of the data spanning 72 hours prior to and 72 hours after the outage, whichever results in more conservative estimate of emission reductions
Greater than one week	No data may be substituted

## 2. Use of a single flow meter for multi-use of recovered biogas

4. If the recovered biogas (e.g. landfill gas) is used for multiple purposes (e.g. flaring or energy generation), and all methane destruction devices are verified to be operational (e.g. by means of flame detectors records, energy generated), a single flow meter may be used to record the flow into multiple destruction devices. The destruction efficiency of the least efficient among the destruction devices shall be used as the destruction efficiency for all destruction devices monitored by this flow meter.
5. If there are any periods for which one or more destruction devices are not operational, emission reductions from methane destruction for these periods may be claimed provided that verification confirms the fulfilment of all the following conditions indicated below. In such a case, the destruction efficiency of the least efficient destruction device in operation shall be used as the destruction efficiency for all destruction devices monitored by this single flow meter:
  - (a) All destruction devices are either equipped with valves on the input gas line that close automatically (e.g., normally closed valves) if the device becomes non-operational (i.e., requiring no manual intervention), or designed in such a manner that it is physically impossible for the gas to pass through and into the atmosphere while the device remains non-operational; and
  - (b) For any period where one or more destruction devices within this arrangement are not operational, it shall be demonstrated that the remaining operational devices have the capacity to destroy the actual gas flow recorded during the period. For devices other than flares, it shall be shown that the output corresponds to the flow of gas (e.g., through mass and/or energy balance).
6. Measurement of methane content shall be conducted immediately downstream of the flow meter, while respecting the installation requirements of the flow meter.

## 3. Use of a sampling method for methane content of landfill gas

7. Methane content of landfill gas can be monitored by sampling, provided that the following conditions are met:
  - (a) The maximum waste treatment capacity of the landfill is 200 tonnes waste per day; and
  - (b) The standard "Sampling and surveys for CDM project activities and programme of activities" is applied for conducting sampling with a minimum sampling frequency of two samples per week; and
  - (c) National or international protocols for measuring methane content of biogas by a semi-continuous analysis shall be followed; otherwise, meter reading can only be

collected when the methane content has reached stabilization for at least 3 minutes. Orsat analysis is not eligible; and

- (d) The biogas flow rate is monitored continuously. The methane content measured by sampling for a given period can be used directly only if the average flow rate during the following week does not fluctuate by more than +/- 20% as compared to the mean value of the flow rates for the period during which the methane content is measured by sampling. Otherwise, a conservative adjustment shall be applied to the measured methane content, i.e. by applying the observed deviation as a discounting factor.

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### Document information

<i>Version</i>	<i>Date</i>	<i>Description</i>
03.0	27 November 2015	EB 87, Annex 10 Revision to provide simplified procedure for mass flow monitoring of methane in biogas.
02.0	3 June 2011	EB 61, Annex 11 Revision to: <ul style="list-style-type: none"> <li>• Corrects inconsistencies in the expression of some parameters;</li> <li>• Provides a more simple option to demonstrate that the gaseous stream is dry based on showing that the temperature of the gaseous stream does not exceed 60°C, and changing the threshold for moisture content for a dry gaseous stream to be equal to or less than 0.05 kg H<sub>2</sub>O/m<sup>3</sup> dry gas;</li> <li>• States that only the volumetric fraction of greenhouse gases being considered in the emission calculation of the underlying methodology must be monitored for determining the molecular mass of the gaseous stream;</li> <li>• Changes the frequency that the moisture content must be monitored to coincide with calibration of the flow meter, or the time of the Annual Surveillance Test associated with the EN 14181;</li> <li>• Editorial changes to improve the tool's structure, incorporate additional cross-referencing and remove repeated text.</li> </ul>
01.0	28 May 2009	EB 47, Annex 10 Initial adoption.

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